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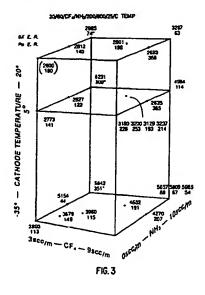
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Reactive ion etch process including hydrogen radicals.

The addition of a gaseous source of hydrogen radicals, such as hydrogen, ammonia or methane to oxide RIE etching chemistries, in amounts of from about 5 to about 20 percent by volume of the total gas flow, will increase the oxide etch rate while suppressing the polysilicon etch rate. This effect is more pronounced at lower wafer temperatures. This new process chemistry increases the oxide etch rate to greater than 5000 Å/min., improves the selectivity to polysilicon to greater than 25:1 and improves the selectivity to photoresist to greater than 6:1, without having a significant detrimental effect on the profile angle, the RIE lag and the etch rate uniformity. Selectivities of 50:1 have been achieved with less than 15% RIE lag using the chemistry CHF₃, Ar, CF₄ and NH₃, with NH₃ constituting 10 percent by volume of the gas flow.



The present invention relates generally to a process for etching dielectric layers in the fabrication of semiconductor devices. More particularly, it relates to such a process for etching oxides. Most especially, it relates to such a process for contact etching, particularly in high aspect ratio geometries.

Reactive ion etch (RIE) processes for etching oxide layers are well known in the art and have achieved wide acceptance in the semiconductor industry. For example, apparatus for carrying out such processes is described in commonly assigned U.S. Patent 4,842,683, issued June 27, 1989 to Cheng et al. and U.S. Patent 4,668,338, issued May 26, 1987 to Maydan et al. Apparatus for carrying out such processes is commercially available from Applied Materials, Santa Clara, California, under the designation Precision 5000E and 8300. Currently, gas mixtures used for etching oxide in the Precision 5000E apparatus include mixtures of CHF₃ and O₂; CHF₃, Ar and O₂; CHF₃, Ar and CF₄; CHF₃, He, and CF₄ and CHF₃, Ar and C₂F₆. These chemistries can achieve high etch rates and high selectivities, but oxide to polysilicon selectivities of greater than 25:1 cannot be achieved without an increase in the RIE lag to greater than 15 percent. The term "RIE lag" refers to the percentage difference in the oxide etch depth of 1 micron (μ) wide contacts compared with the oxide etch depth of 0.5 μ wide contacts under the same process conditions.

In detailed studies of the standard oxide etch chemistry of CHF3, Ar and CF4 and standard 5000E apparatus for a high aspect ratio contact etch, it was determined that there would be difficulty meeting the following specification:

RIE Lag Etch Rate Uniformity Selectivity	<10% in 0.5 µm contacts compared with 1.0 µm contacts at 2.0 µm depth. >4000 Å/min, undoped oxide <10% 3σ, 6mm edge exclusion >30:1 to doped polysilicon
Profile	>85 degrees.

It was found that there is always a compromise between lag and selectivity. The etch rate, uniformity and profile specifications can be achieved over a large process window, but it is hard to achieve a selectivity greater than 20:1 with a lag of less than 10%. This is also true for cathode temperatures as low as -40 °C. At such lower cathode temperatures, the process window is reduced further because the profile angle is worse due to increased polymer deposition.

The addition of a gaseous source of hydrogen (H and/or H₂) radicals, such as hydrogen, ammonia or methane to oxide RIE etching chemistries, desirably in amounts of from about 5 to about 20 percent by volume of the total gas flow, will increase the oxide etch rate while suppressing the polysilicon etch rate. This effect is more pronounced at lower wafer temperatures. This new process chemistry increases the oxide etch rate to greater than 5000 Å/min., improves the selectivity to polysilicon to greater than 25:1 and improves the selectivity to photoresist to greater than 6:1, without having a significant detrimental effect on the profile angle, the RIE lag and the etch rate uniformity. Selectivities of 50:1 have been achieved with less than 15% RIE lag using the chemistry CHF₃, Ar, CF₄ and NH₃, with NH₃ constituting 10 percent by volume of the gas flow. For purposes of this invention, the term "reactive ion etch" refers to plasma etching processes which have a DC bias on a substrate holder, thus giving ion bombardment on the substrate.

A reactive ion etch process in accordance with this invention includes positioning a structure comprising at least one of a dielectric layer and a semiconductor layer on a surface of a substrate in a closed chamber. A selected reactive gas mixture including a gaseous source of hydrogen radicals is supplied to the chamber. RF energy is supplied to the chamber to establish an etching plasma and an associated electric field substantially perpendicular to the surface of the substrate. A DC magnetic field is applied to the chamber substantially perpendicular to the electric field and parallel to the surface of the substrate. The reactive gas mixture is allowed to etch at least a portion of the dielectric or semiconductor layer.

The attainment of the foregoing and related advantages and features of the invention should be more readily apparent to those skilled in the art, after review of the following more detailed description of the invention, taken together with the drawings, in which:

Figure 1 is a perspective view of a plasma etching system suitable for practice of the invention.

Figure 2 is a cross section view of the plasma etching system of Figure 1.

Figure 3 is a graph of results obtained with practice of a reactive ion tch process in accordance with the invention.

Turning now to the drawings, more particularly to Figures 1 and 2, there is shown an RIE mode plasma etching system 60 which can be used to practice the process of the present invention. The system 60 includes a housing 62, typically of non-magnetic material, such as aluminum, which has an octagonal

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configuration of outer walls 64. Circular inner wall 66 defines etch chamber 68. The reactor system 60 also includes a unique gas- and liquid-cooled pedestal/cathode assembly 70 and a wafer exchange system 74.

The wafer exchange system 74 includes vertically movable wafer lift fingers 79 which pick up a wafer 75 from an external manually held of operated blade 76 which is inserted into the chamber or, preferably, from an external load lock robot blade 76, and transfer the wafer to the cathode 72 for processing, then return the processed wafer to the robot blade for removal from the chamber.

In addition, the wafer exchange system 74 integrally incorporates a wafer clamp ring 78 with wafer lift fingers 79. The design of the wafer exchange system 74 and the incorporation of the associated wafer lift and clamping structures permit the use of a one-axis robotic drive within the chamber. Furthermore, the operation of the chamber robot requires that the external robot merely present the wafer to a selected transfer position for exchange with the chamber robot. Simplifying the demands on the external robot makes possible a relatively simple robot, even when the robot is used in a multi-chamber load lock system that serves a multiplicity of reactors.

Process gases are supplied to the interior of the chamber 68 by a gas manifold 80 from a gas supply system 81 comprising one or more gas storage reservoir/tanks. The gas supply system 81 communicates to the manifold 80 and chamber 68 via supply line(s) 82, which is coupled into the manifold 80 by inlet connection 84. The system includes an automatic flow control system or other suitable control system which controls the flow rates of the various etchant gases, carrier gases, and the like, supplied to the chamber 68.

Vacuum is supplied to the chamber and spent gases and entrained products are exhausted via annular exhaust chamber 90 communicating to exhaust port 92, which, in turn, is connected to a conventional vacuum pumping system 93. The exhaust flow is directed from the chamber 68 through holes 94 in a horizontal annular plate 96 mounted about the upper periphery of the cylindrical cathode assembly 70. Tile apertured plate 96 inhibits plasma penetration into the annular exhaust chamber 90. This exhaust arrangement facilitates uniform coverage and etching of wafer 75 by the reactant gas. Control of the exhaust system can be by a capacitive conventional system, such as a manometer sensor (not shown), which operates through a pressure control system and D.C. motor to control the speed of the blower, or by other conventional control systems.

As indicated by the arrows 102, 104, 106, 108 in Figure 2, the gas communicated by inlet 84 (arrow 100) is routed into the manifold 80 (arrow 102) and is then directed downwardly from the manifold (arrow 104), forming an etching gas plasma in chamber process region 110 during application of RF power, then flows over the wafer 75 and radially outwardly across the wafer and into the annular exhaust chamber (arrow 106), then out the exhaust port 92 (arrow 108).

The above-mentioned RF power is supplied by an RF supply system 112 to the reactor system 60 for plasma operation, i.e., to create an etching gas plasma from the inlet gases in process region 110. This system 112 includes an RF power supply and a load matching network, and is connected to the pedestal 72, with the chamber walls being at ground. That is, the pedestal is the powered cathode. The RF power typically is supplied at a high frequency, preferably about 13.6 MHz. However, the reactor system 60 can be operated at low frequencies of, for example, several KHz.

The use of a powered pedestal cathode 72 has the advantage of concentrating the RF power and plasma on the surface area of the wafer and increasing the power density across the wafer while reducing it everywhere else. This ensures that etching takes place on the wafer only, reducing erosion in other parts of the chamber, and thus reducing possible wafer contamination. Typically, power densities of about 2.5-3.5 watts/cm² are and can be used. These high power densities require cooling. Preferably, the RF-powered cathode 72 is constructed to combine gas-enhanced wafer-to-cathode thermal conductance and liquid cathode cooling. However, the application of cooling gas, such as helium, to the powered pedestal 72 at low pressure would ordinarily cause the cooling gas to break down. The reactor system 60 includes a unique gas feed-through 114 that supplies the gas to the high voltage electrode without ionization. Further details on the construction and operation of the system 60 are provided in the above referenced Cheng et al., U.S. Patent 4,842,683, the disclosure of which is incorporated by reference herein. Alternatively, an RIE mode plasma etching system as described in the above-referenced Maydan et al., U.S. Patent 4,668,338, could be employed, the disclosure of which is also incorporated by reference herein.

Standard system configurations used for REI etching of oxides, such as systems incorporating electron cyclotron resonance (ECR) and inductive and capacitive RF sources and the like are operable with the process of this invention. Suitable gaseous sources of hydrogen radicals include hydrogen gas, which is preferably supplied in admixture with an inert carrier gas, such as helium or argon, desirably in an amount of about 10 volume percent hydrogen gas, balance inert carrier gas, ammonia and methane. The preferred gaseous source of hydrogen radicals is ammonia.

The following table shows suitable ranges and optimum values for 5 inch silicon wafers for use of the invention with a preferred reaction chemistry:

Variable	Range	Optimum, 5" Wafers					
CHF₃	10-100 scc/m	30					
Ar	50-200 scc/m	60					
CF.	3-20 scc/m	3					
Pressure	5-500 mT.	200					
Power	400-1200 watts	600					
B field	0-120 gauss	25					
Temperature	0-20 °C - standar	d refrigeration					
	-40-20 °C - with special refrigeration						

The following non-limiting examples represent best modes contemplated by the inventors for practicing the invention and describe the invention further.

Example 1

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Different reaction gas chemistries were investigated in the 5000E system to find a process which would provide higher selectivity without increasing the RIE lag. The chemistries studied were:

- 1. CHF3, Ar and SF6;
- 2. CHF₃, Ar and C₂F₆ and
- 3. CHF₃, Ar, CF₄ and NH₃

The following reaction conditions were used: 30 sccm CHF $_3$ / 60 sccm Ar / 3 sccm SF $_6$ / 0 sccm NH $_3$ / 200 mT / 600 W / 25 G / 20 °C; 30 sccm CHF $_3$ / 60 sccm Ar / 3 sccm C $_2$ F $_6$ / 0 sccm NH $_3$ / 200 mT / 600 W / 25 G / 20 °C.; 30 sccm CHF $_3$ / 60 sccm Ar / 3 sccm CF $_4$ / 10 sccm NH $_3$ / 200 mT / 600 W / 25 G / 20 °C.

Swapping CF₄ for SF₆ reduced the selectivity by about a factor of two using the same CF₄ and SF₆ flow, and so this chemistry was rejected. Swapping CF₄ for C₂F₆ had little effect on the etch rates and selectivity with the same CF₄ and C₂F₆ flow. Changing the Ar:CHF₃ gas flow ratio and pressure still did not show any significant difference between the CHF₃, Ar and C₂F₆ and CHF₃, Ar and CF₄ chemistry was not examined any further. However, the addition of NH₃ to the CHF₃, Ar and CF₄ chemistry was found to have significant benefits, especially at low cathode temperatures. Similar results should be obtained with the addition of NH₃ to the other two chemistries. The addition of NH₃ increases the profile angle, and can increase the selectivity without increasing the lag. The following specifications are achievable:

RIE Lag Etch Rate Uniformity Selectivity	<14% in 0.5 μm contacts at 2.0 μm depth. >3000 Å/min, undoped oxide. <12% 3σ, 6 mm edge exclusion. >30:1 to deped polysilican.
Selectivity Profile	>30:1 to doped polysilicon. >85 degrees.

Significant polymer deposition is observed, which may present a particle problem.

Example 2

Further study of NH₂ addition was carried out, by adding NH₃ to the reactant gas in a commercial process using the following conditions:

30 sccm CHF₃/60 sccm Ar / 3 sccm CF₄ / 0 sccm NH₃ / 200 mT / 600 W / 25 G / 20 ° C.

The experiment examined the effects of CF₄ and NH₃ flow, as well as the cathode temperature. The experiment included runs with a 5 °C cathode temperature to allow operation of the 5000E system with standard hardware. The parameter space studied is as follows:

Factor	Low	Center	High
CHF _{3:}		30 scc/m	
Ar:		60 scc/m	
CF4	3 scc/m		9 scc/m
NH ₃	0 scc/m		10 scc/m
Pressure		200mTorr	
Power		600 Watt	
B Field		25 gauss	
Cathode Temp:	-35 · C		20 · C

The results are shown in Figure 3. To summarize the results, when 10 scc/m of NH₃ is used, the oxide etch rate increases by up to 100% when the cathode temperature is reduced from 20 °C to -35 °C. If no NH₃ is added, the oxide etch rate increases by 10%, at most, with the same change in cathode temperature. The polysilicon etch rate is controlled by the ratio of CF₄ and NH₃ flows. With the CF₄ flow higher than the NH₃ flow the polysilicon etch rate is high, but with NH₃ flow higher than the CF₄ flow the polysilicon etch rate is lower. However, in the latter case, a thick layer of polymer can be deposited, which can affect the Nanospec interferometer readings of polysilicon thickness. Selectivities of up to 100:1 have been achieved with 10 scc/m of NH₃ and -35 °C cathode temperature.

A number of runs were also made with lower pressure and higher Ar:CHF₃ flow ratios. The following three runs had polysilicon etch rates of about 2500 Å/min:

Process	units	1	2	3
CHF ₃	scc/m	10	10	30
Ar	scc/m	80	80	60
CF4	scc/m	3	9	9
NH₃	scc/m	10	10	10
Pressure	mTorr	200	200	70
Power	Watts	600	600	600
B Field	gauss	25	25	25
Cathode Temp	Celsius	20	20	20

Example 3

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Based on Example 2, it was decided to conduct a screening experiment to determine the most important factors affecting the oxide and polysilicon etch rates. The experiment used an L8 Taguchi screening design with one center point and the following levels:

units	low	center	high
scc/m:scc/m	2	3	4
scc/m	3	6	9
scc/m	4	7	10
mTorr	150	200	250
Watts	600	700	800
gauss	25	50	75
Celsius	-35	-7.5	20
	scc/m:scc/m scc/m scc/m scc/m mTorr Watts gauss	scc/m:scc/m 2 scc/m 3 scc/m 4 mTorr 150 Watts 600 gauss 25	scc/m:scc/m 2 3 scc/m 3 6 scc/m 4 7 mTorr 150 200 Watts 600 700 gauss 25 50

The results are shown in the following table:

35	30	25		20		15	10		5	
Process #	Units	-	2	m	বা	v.	g	7	oci	-1
CHF ₃	scem	30	81	30	2 2	30	×	30	<u>×</u>	23
Ar	sccm	09	72	09	72	09	72	. 99	72	67
CF4	sccm	3	3	6	6	8	٣	2	2	9
NII,	sccm	4	4	4	7	91	2	9	2	7
Pressure	mTorr 150	150	250	250		250	150	150	250	200
Power	Watts	800	009	909		800	009	009	800	2(8)
B Field	ganss	75	25	75	25	25	7.5	25	7.5	90
Temperature	ڼ	20	50	-35	-35	-35	-35	20	20	-7.5
Ox Time	sec.	3	99	9	99	3	9	9	9	ę
Poly Time	sec.	120	120	120	120	120	120	120	120	130
Thermal Oxide	Å/min. 5093	.5093	2667	4111	1234	6128	8.1.17	3398	52.42	4559
Oxide Uniformity	<u>max./min</u> 4.6 2 x mean	4.6	4.9	2.9	3 0.	5.4	0.0	2.4	æ.	~; `
Polysilicon	Å/min. 299	. 299	231	517	565	83	4804	218	643	284
Polysilicon Uniformity	max./min 14.9 2 x mean	14.9	6.2	4.9	16.8	13.0	83.2	5.0	5.1	38.3

45 Analysis of the data shows that NH₃ flow, cathode temperature, B field and CF₄ flow are the most important factors controlling the oxide etch rate. This agrees with the results of Example 1 except for the effect of CF₄ flow. Decreasing oxide etch rate with increasing CF₄ flow is also contrary to the behavior of CHF₃/Ar/CF₄ chemistry. Similarly, power is one of the least important factors affecting etch rate with the addition of NH₃, quite different from the behavior of CHF₃/Ar/CF₄ chemistry. The results confirm that the addition of NH₃ to the CHF₃/Ar/CF₄ chemistry can either decrease or significantly increase the polysilicon etch rate. The sensitivity of the polysilicon etch rate with different Ar:CHF₃ flow ratios and pressures is much less without NH₃ in the gas mixture.

Example 4

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A screening experiment was designed to determine the effect of NH₃ addition on RIE lag and profile angle in a limited parameter space. The experimental design was a fractional factorial with two center points, four factors, ten runs.

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Factor	Units	Low	Center	High
Total Flow Ar:CHF3 CF4 NH3 Pressure Power B Field	scc/m scc/m scc/m mTorr Watts gauss	80 1 5 5	100 2 7 7 200 700 25	120 3 9 9
Cathode Temp	Celsius		-35	

The results are shown in the following table:

15	의	29	57	7	7	200	700	25	-35	99	081	-10-19	4.9	204		 8		2.60
20	6	29	57	7	7	200	200	25	-35	9	<u>8</u>	1764		218	5500	1.15	280	2.55
	∽	27	08	5	2	200	700	25	-35	99	<u>9</u>	5736	6.9	223	6300	1.40	230	2.40
25	7	11	. 65	6	S	200	200	25	-35	09	081	4208	5.9	417	4900	1.16	314	2.55
	9	53	53	6	2	200	200	25	-35	99	180	4000	5.6	172	4600	1.15	330	2.52
30	~	31	31	6	6	200	.700	25	-35	09	180	5415	5.5	214	0009	1.11	244	2.42
35	41	28	83	S	5	200	200	25	-35	9	180	4677	4.7	172	5000	1.17	282	2.32
	cal	11	20	2	5	200	700	25	-35	09	180	7258	4.8	3300	0069	0.95	182	2.10
40	7	53	53	2	9	200	200	25	-35	99	180	68.38	4. 1.	41	6400	0.94	961	2.10
	1	35	35	2	2	200	700	25		99	180	. 4077	1.5.8	. 215	Å/min. 4800	1.18	324	micron 2.60
45	Units	sccm	scem	sccm	sccm	mTorr	Watts	gauss	ڹ	<u> ۲</u> ۲.	Scc.	Å/min. 4077	max./min.5.8 2 x mean	Å/min. 215	Å/min	ratio	sec.	micro
50									lure		2	Oxide	Oxide Uniformity 1	uo.	SOS	χ̈́	บ	1.0 Micron Depth
55	Process #	CHF3	γı	CF.	NII,	Pressure	Power	B Field	Temperature	Ox Time	Poly Time	Thermal Oxide	Oxide Ui	Polysilicon	HAR TEOS	IIAR/I.Ox	Etch Time	1.0 Micr

	27.0 13 84
5	25.2
	28.3
10	1.8 1.8 1.8
16 .	26.7 21 79
	28.0 13 82
20	29.1 18 81
	2.1
25	156.1 18 82
<i>30</i>	0xide/poly22.3 156.1 2.1 (%) (0.5/1.0) 21 18 12 (°,1.0) 78 82 89
40	sclectivity HE Lag rofile Angle

45 In the parameter space studied, higher NH₃ flow improves oxide etch rate, selectivity, RIE lag and profile angle. Some further checks were made to confirm the trends observed, with the results shown in the following table.

Process	units	1	2	3	4
CHF₃	scc/m	20	20	30	30
Ar	scc/m	45	45	60	60
CF4	scc/m	7	9	9	7
NH ₃	scc/m	7	9	9	7
Pressure	mTorr	200	200	200	200
Power	Watts	600	600	600	600
B Field	gauss	25	25	25	25
Cathode Temp	·c	-35	-35	-35	-35
Oxide Etch Rate	Å/min	6000	6300	6300	5500
Profile		85	85	85	83
Lag (0.5μm/1.0μm)		~13%	<13%	-12%	<17% -@ 2µm Depth

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Example 5

Process #1 in the above table was ran again to check the selectivity to silicon at the bottom of a contact. The aspect ratio of 0.5µm contacts is 6.4. About 1200 Å of silicon has been etched in a trench during approximately 270 seconds, giving a rate of about 260 Å/min. and a selectivity of about 22:1.

Substitution of 10 volume percent hydrogen in helium or argon, or methane, in the procedures of the above examples in equivalent amounts will give similar advantageous results.

It should further be apparent to those skilled in the art that various changes in form and details of the invention as shown and described may be made. It is intended that such changes be included within the spirit and scope of the claims appended hereto.

Claims

- 1. A reactive ion etch process, which comprises positioning a structure comprising at least one of a dielectric layer and a semiconductor layer on a surface of a substrate in a closed chamber, supplying a selected reactive gas mixture including a gaseous source of hydrogen radicals to the chamber, applying RF energy to the chamber to establish an etching plasma and an associated electric field substantially perpendicular to the surface of the substrate, applying a DC magnetic field to the chamber substantially perpendicular to the electric field and parallel to the surface of the substrate, and allowing the reactive gas mixture to etch at least a portion of the dielectric or semiconductor layer.
 - 2. The reactive ion etch process of Claim 1 additionally comprising the steps of applying a masking layer to the dielectric or semiconductor layer and forming at least one opening in the masking layer to expose the dielectric or semiconductor layer in the at least one opening.
 - 3. The reactive ion etch process of Claim 1 in which the gaseous source of hydrogen radicals comprises hydrogen, ammonia or methane.
- 4. The reactive ion etch process of Claim 3 in which the gaseous source of hydrogen radicals comprises
 - 5. The reactive ion etch process of Claim 4 in which the reactive gas mixture contains from about 5 to about 20 percent by volume of ammonia.
- The reactive ion etch process or Claim 5 in which the reactive gas mixture contains about 10 percent by volume ammonia.
- 7. The reactive ion etch process of Claim 4 in which the reactive gas mixture additionally comprises CHF₃ and argon.
- The reactive ion etch process of Claim 7 in which the reactive gas mixture additionally comprises CF₄ or C₂F₆.

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- 9. The reactive ion etch process of Claim 1 in which the dielectric layer is a silicon oxide layer.
- 10. The reactive ion etch process of Claim 1 in which the semiconductor layer is a silicon layer.
- 11. The reactive ion etch process of Claim 1 in which the substrate is positioned at a cathode of the chamber, the process additionally comprising the step of establishing a temperature between about -40 degrees Centigrade and about 20 degrees Centigrade at the cathode prior to allowing the reactive gas mixture to etch at least a portion of the dielectric or semiconductor layer.
- 12. The reactive ion etch process of Claim 11 in which a temperature between about 0 degrees Centigrade and about 20 degrees Centigrade is established.
 - 13. In a reactive ion etch process for etching a dielectric or a semiconductor, the improvement which comprises adding a gaseous source of hydrogen radicals to a reactive gas mixture in an amount sufficient to increase at least one of etch rate and selectivity of the reactive gas mixture for the dielectric or the semiconductor.
 - 14. The reactive ion etch process of Claim 13 additionally comprising the steps of applying a masking layer to the dielectric or semiconductor layer and forming at least one opening in the masking layer to expose the dielectric or semiconductor layer in the at least one opening.
 - 15. The reactive ion etch process of Claim 13 in which the gaseous source of hydrogen radicals comprises hydrogen, ammonia or methane.
- 25 16. The reactive ion etch process of Claim 15 in which the gaseous source of hydrogen radicals comprises ammonia.
 - 17. The reactive ion etch process of Claim 16 in which the reactive gas mixture contains from about 5 to about 20 percent by volume of ammonia.
 - 18. The reactive ion etch process of Claim 17 in which the reactive gas mixture contains about 10 percent by volume ammonia.
- The reactive ion etch process of Claim 16 in which the reactive gas mixture additionally comprises
 CHF₃ and argon.
 - 20. The reactive ion etch process of Claim 19 in which the reactive gas mixture additionally comprises CF₄ or C₂F₆.
- 40 21. The reactive ion etch process of Claim 13 in which the dielectric layer is a silicon oxide layer.
 - 22. The reactive ion etch process of Claim 13 in which the semiconductor layer is a silicon layer.
- 23. The reactive ion etch process of Claim 13 in which the substrate is positioned at a cathode of the chamber, the process additionally comprising the step of establishing a temperature between about -40 degrees Centigrade and about 20 degrees Centigrade at the cathode prior to allowing the reactive gas mixture to etch at least a portion of the dielectric or semiconductor layer.
- 24. The reactive ion etch process of Claim 23 in which a temperature between about 0 degrees Centigrade and about 20 degrees Centigrade is established.

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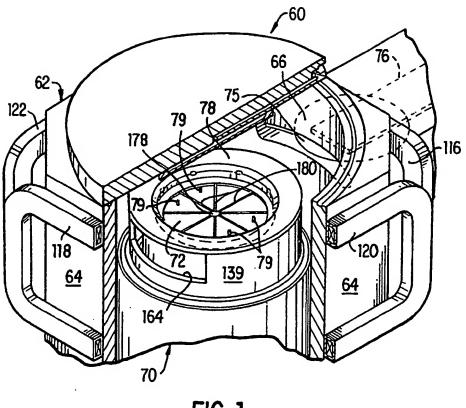


FIG. 1

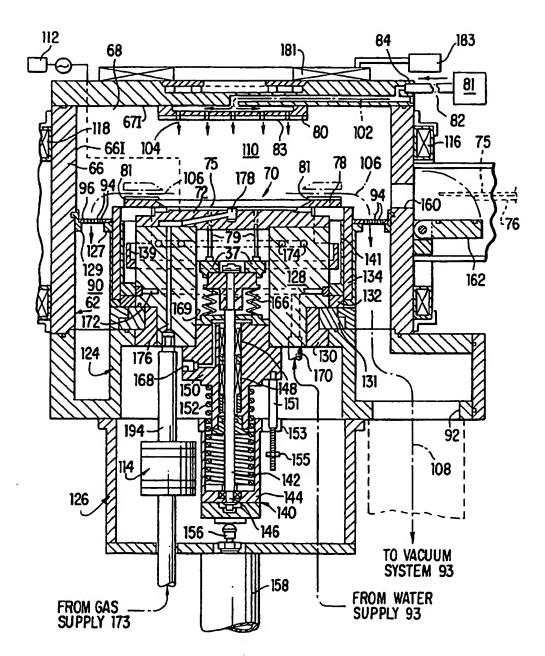


FIG. 2

30/60/CF4/NH3/200/600/25/C TEMP

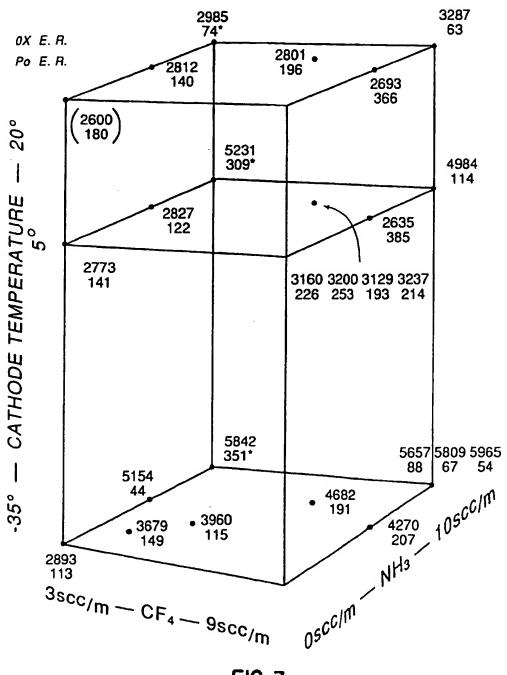


FIG. 3



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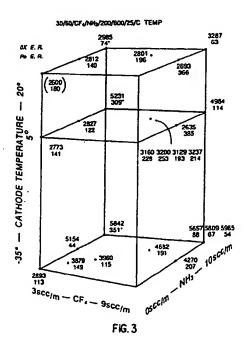
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- Reactive ion etch process including hydrogen radicals.
- (57) The addition of a gaseous source of hydrogen radicals, such as hydrogen, ammonia or methane to oxide RIE etching chemistries, in amounts of from about 5 to about 20 percent by volume of the total gas flow, will increase the oxide etch rate while suppressing the polysilicon etch rate. This effect is more pronounced at lower wafer temperatures. This new process chemistry increases the oxide etch rate to greater than 5000 A/min., improves the selectivity to polysilicon to greater than 25:1 and improves the selectivity to photoresist to greater than 6:1, without having a significant detrimental effect on the profile angle, the RIE lag and the etch rate uniformity. Selectivities of 50:1 have been achieved with less than 15% RIE lag using the chemistry CHF3, Ar, CF4 and NH₃, with NH₃ constituting 10 percent by volume of the gas flow.





EUROPEAN SEARCH REPORT

Application Number EP 93 30 0163

Category	Citation of document with of relevant	indication, where appropriate,	Relevant to claim	CLASSIFICATION OF THE APPLICATION (IncCLS)
X	1 (REGULAR PAPERS vol. 21, no. 5, Ma pages 696-701, OKANO H ET AL 'Re of SiO2 and poly-Sand BF3 gases' * page 696, right page 697, left coll *			H01L21/311 H01L21/321
A			1-8,11, 12 8,23,24	
x	EP-A-0 212 585 (IB		13-17, 21,22	
A	* column 6, line 1	8 - line 36 * - line 4 * 2 - line 16 * 0 - line 49; figure 2 * 4 - line 23 * 5 - column 7, line 3 * - line 4; claims	1-5,9,10	TECHNICAL FIELDS SEARCHED (Int.CL.5) HO1L
	The present search report has	been drawn up for all claims Date of completion of the search		Economy
	BERLIN	21 July 1995	Klop	ofenstein, P
X : parti Y : parti	ATEGORY OF CITED DOCUME calarly relevant if taken alone calarly relevant if combined with an ment of the same category	E : earlier patent do	cument, but publis ate a the application	invention theil on, or



EUROPEAN SEARCH REPORT

Application Number EP 93 30 0163

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Category	Citation of document with of relevant p	indication, where appropriate, assages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (InLCL5)
x	US-A-4 283 249 (LI	NDA M. EPHRATH)	13-18, 21,22	
	* column 4, line 6: * column 5, line 4:	5 - line 26 * 0 - column 4, line 18 * 7 - column 5, line 2 * 7 - column 6, line 28 * 4 - column 8, line 2;		
Y	claims 1,2,6,9,10,		4-6	
^			1-3, 7-12,19, 20,23,24	
x	US-A-4 857 140 (LEE	•	13-16, 19,20,22	
	* column 4, line 19 * column 5, line 10 * column 5, line 49 * column 7, line 18 2A-2D *	5 - line 28 *		
	* column 8, line 7 3A-3C * * column 9, line 2 1,8,9,14 *	-		TECHNICAL FIELDS SEARCHED (Int.QLS)
Y A	1,0,3,17		1-4,7,8 5,6,10, 17,18	
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O : DOD-	written disclosure mediate document	& ; member of the sa document	me patent family	, corresponding



EUROPEAN SEARCH REPORT

Application Number EP 93 30 0163

Category	Citation of document with of relevant p	indication, where appropriate,	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int.CLS)
X A	US-A-4 324 611 (DIA * column 1, line 5 * column 1, line 30 * column 2, line 3 * column 2, line 3	ANE C. VOGEL ET AL.) - line 8 * 5 - line 49 * - line 5 *	13-15, 21,23,24 11,12 1-3, 7-10,19, 20,22	
X	* page 2, line 7 - * page 3, line 26 - * page 4, line 22 - figures 1,2 * * page 6, line 15 - * page 7, line 14 - 4 *	- line 37 * - page 5, line 35; - page 7, line 4 * - page 8, line 8; figur	10,13, 15,21,22	TECHNICAL PIELDS SEARCHED (Int.Cl.5)
A	* page 9, line 24 * page 10, line 12 *	- page 10, line 6 * - line 26; claims 1-4,	7 2,4-7, 11,12, 14, 16-19, 23,24	
	The present search report has I	oces drawn up for all claims Data of completion of the search		Domolaci
	BERLIN	21 July 1995	K10	pfenstein, P
X : part Y : part door A : tech	CATEGORY OF CITED DOCUME icularly relevant if taken alone icularly relevant if combined with an imensi of the same category unlogical background written disclosure	NTS T: theory or print E: earlier patent after the filling other D: document cite L: document cite	iple underlying the focument, but publ	invention ished on, or

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X	* column 1, line 5 * column 1, line 4 * column 2, line 19 * column 2, line 20	4 - line 55 * 5 - line 20 * 6 - line 50 * 7 - line 57; figure *	13-17, 21,22	
A			1-5,7,9, 10	
X	* column 1, line 5 * column 1, line 20 * column 2, line 33 * column 3, line 42	0 - line 27 * 1 - line 46 * 2 - line 48 * 1 - column 4, line 21 * 7 - column 5, line 43;	1,2,9-12	
^	CIGIES 1,2,0,7 3,1	1 14,10,20	7,8,13, 14,19-24	TECHNICAL PIELDS SEARCHED (LDLCL5)
X	AL.) * column 1, line 9 * column 2, line 2 * column 2, line 3	- line 16 *	13-18,21	
A		-/	1-7,9,19	
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Ρ,Χ	EP-A-0 498 209 (SO	NY CORP.)	13-15,	
	* column 1, line 1		21,22	
	* column 1, line 1 * column 2, line 4			
	* column 3. line 3	4 - column 4, line 5 *		
		5 - column 7, line 9 *		
	* column 12, line	5 - line 11; claims 1-4;		
	figures 1A-1C *			
P,A			1-3,9,1d	
D,A	US-A-4 668 338 (DA		1,7-10, 13,19-22	
	* column 1, line 5	- column 10 *	13, 13-22	
	* column 4. line 2	1 - line 65; figure 4 *		
	* column 5, line 1	3 - line 19 *		
	* column 5, line 2	5 - line 44 *	ļ	
	* column 6, line 3	2 - line 45 *		
	r column 7, line 6	1 - line 66; figure 8 *	ł	
	* column 8, line 2	- cc 9nrı - +	İ	
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Y:pur	icularly relevant if taken alone icularly relevant if combined with an	after the filing date other D: document cited in t	the application	
A : (ect	ment of the same category nological background	L : document cited for	or other reasons	
O : 200	-written disclosure	& : member of the same	e patent family	, corresponding